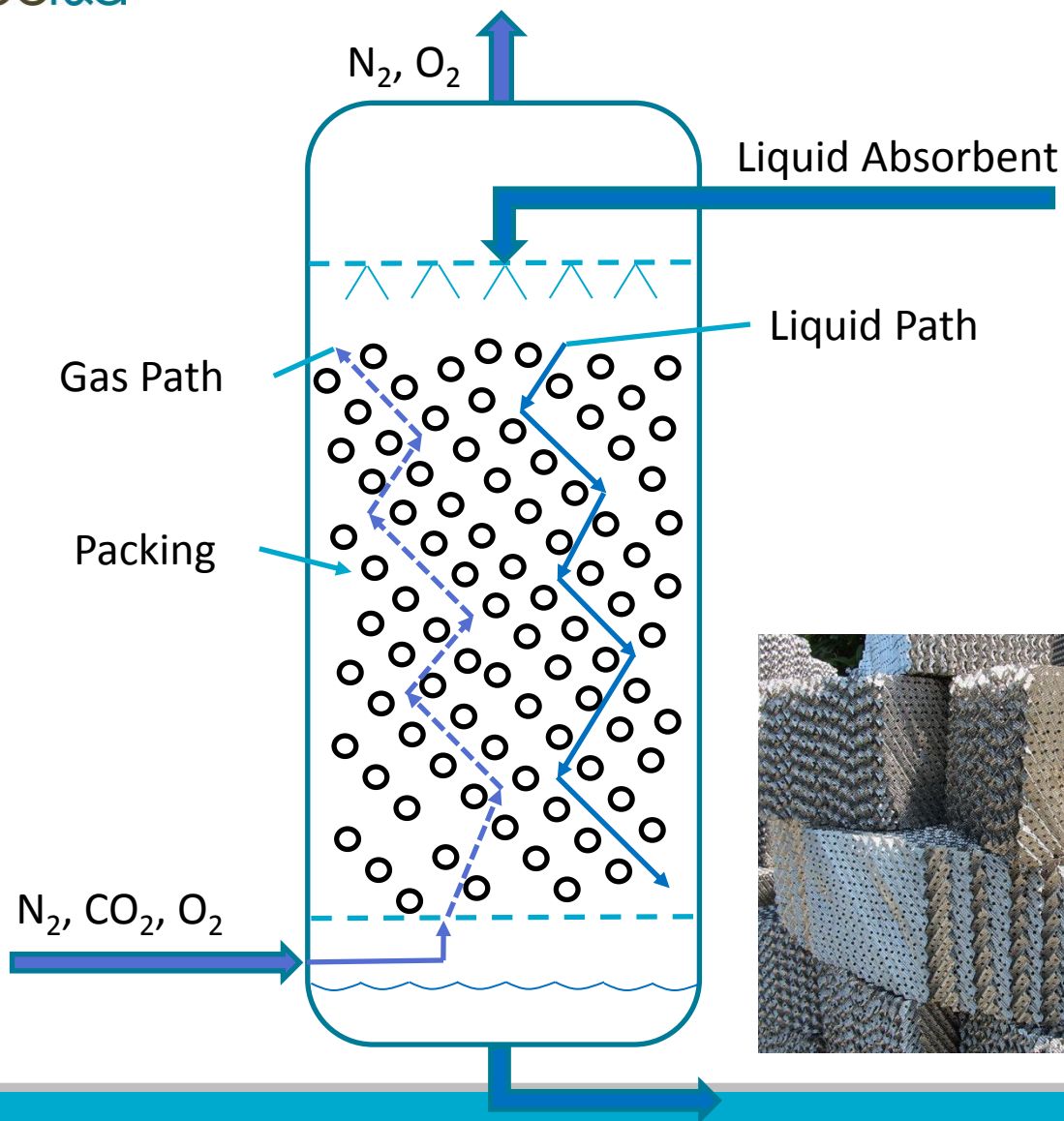


The physical process

- Gas-liquid contacting
- Mass transfer in packed columns
- CO₂ stripping

Gas-liquid contacting: PACKED COLUMNS



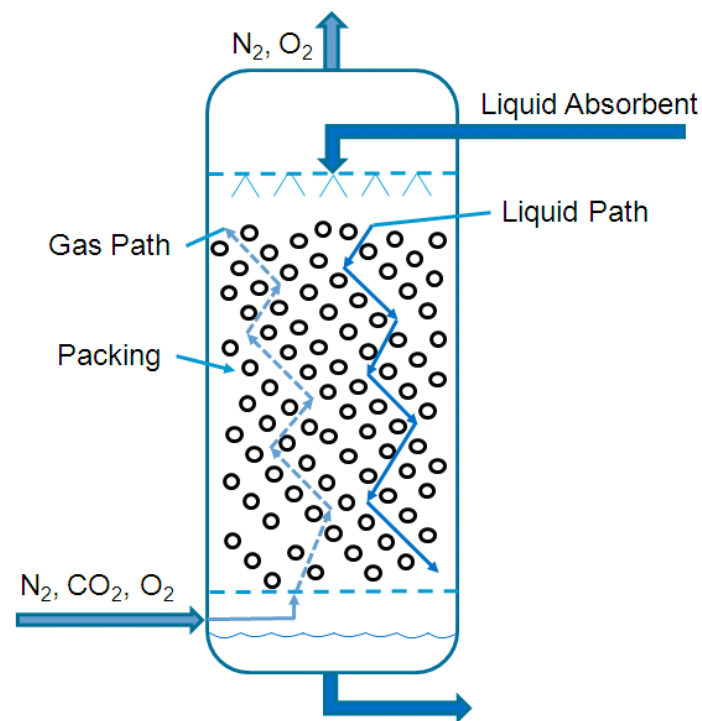
Random Packing



Structured Packing

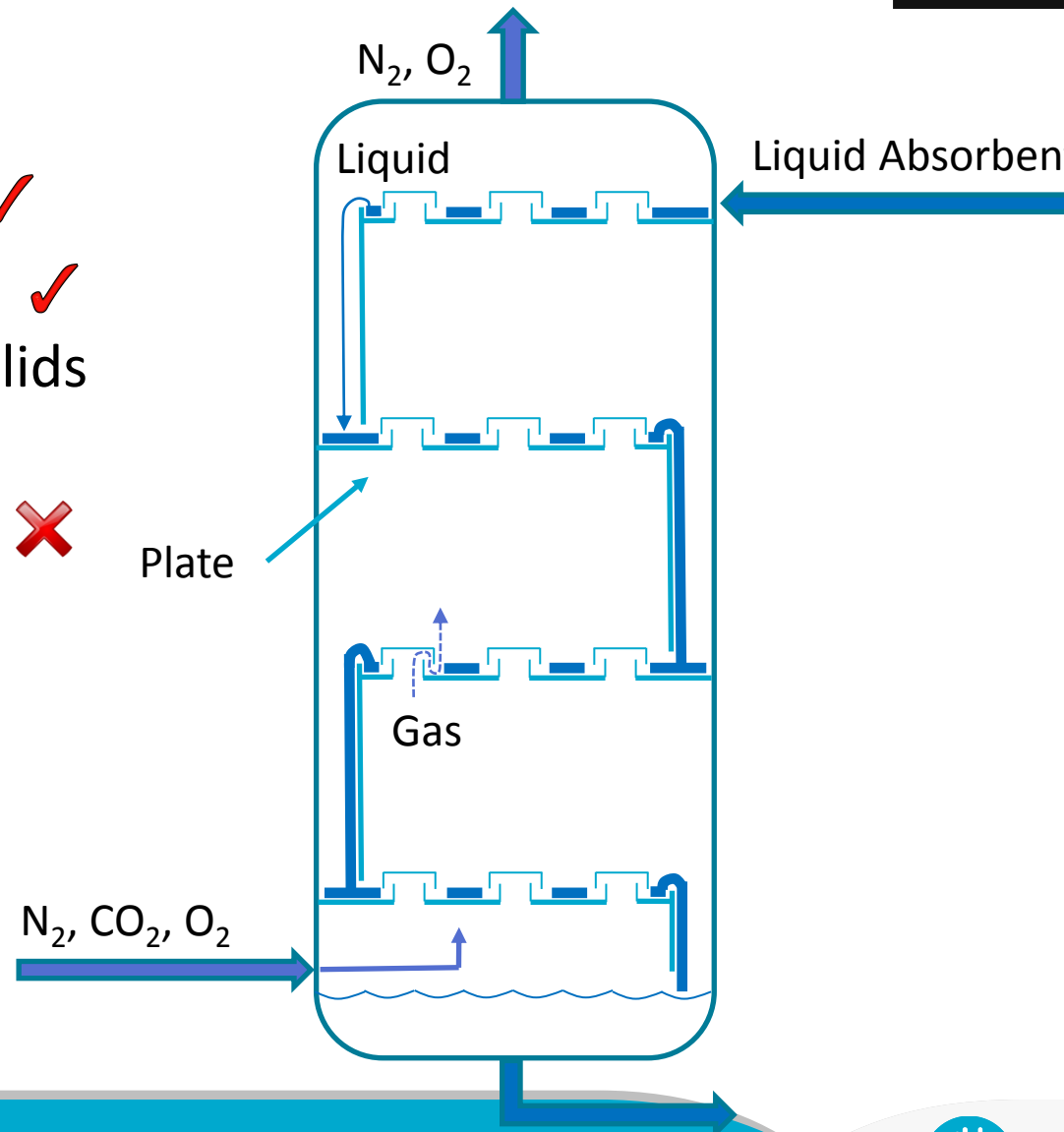


- Packing provides the contact area ✓
- Low liquid hold-up ✓
- Low gas-side pressure drop ✓
- Moderate liquid residence time ✓
- Not suitable for liquids with solids present ✗



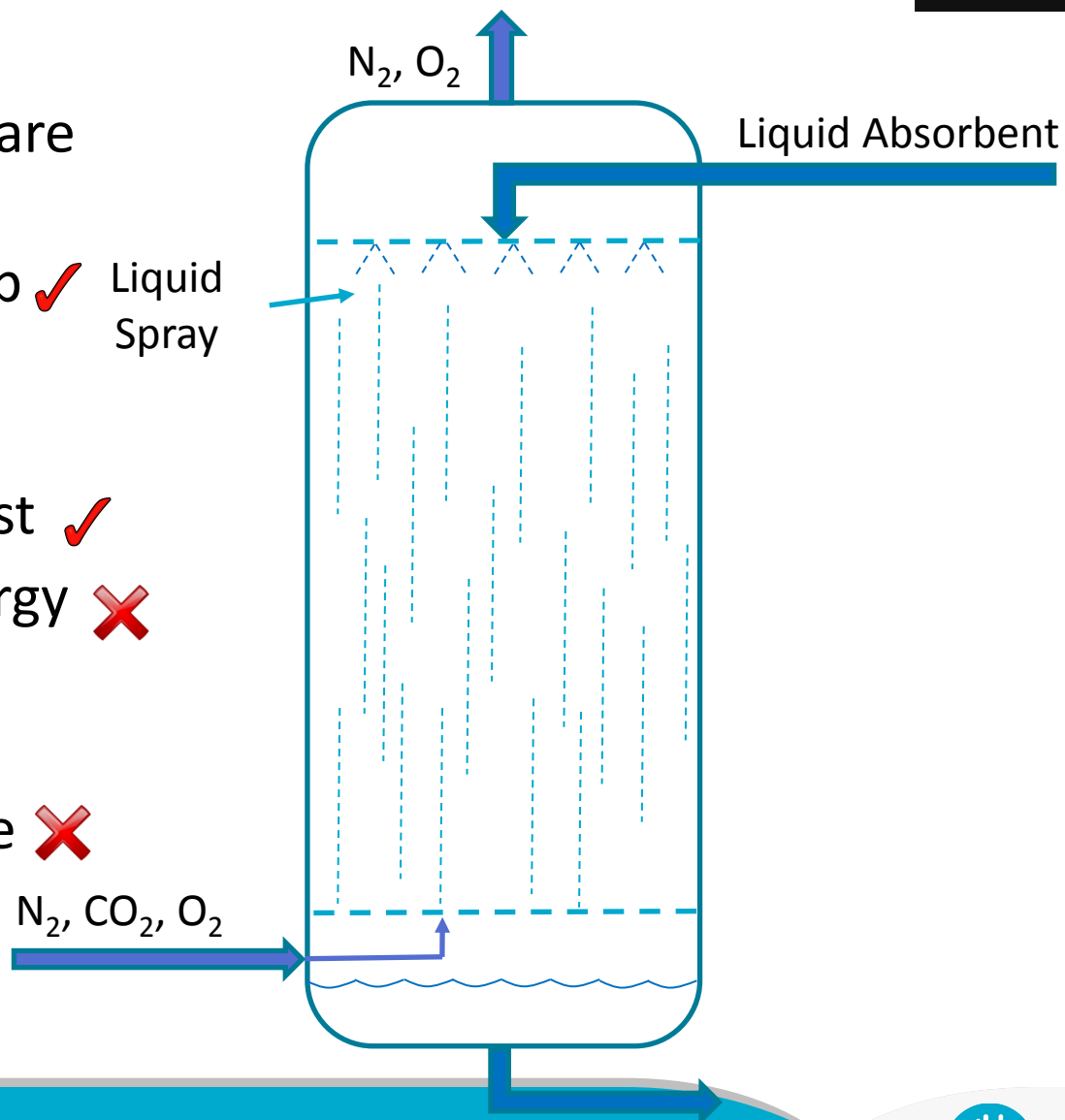
Gas-liquid contacting: PLATE COLUMNS

- Long residence time and complete mixing on plates ✓
- Intermediate liquid hold-up ✓
- Can work for liquids with solids present ✓
- High gas-side pressure drop ✗
- High capital cost ✗



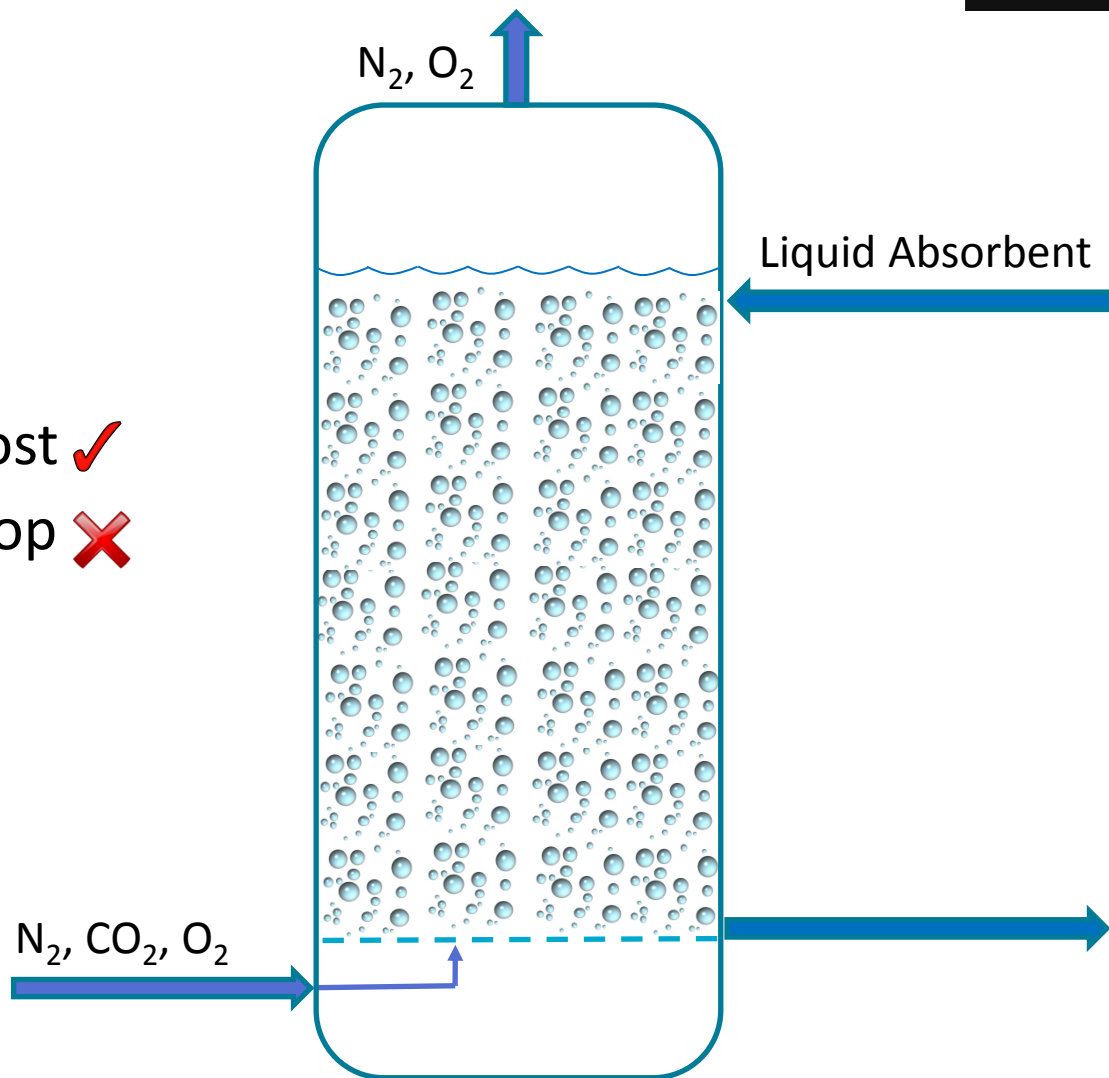
Gas-liquid contacting: SPRAY COLUMNS

- The liquid and gas phases are dispersed
- Low gas-side pressure drop ✓
- Suitable for liquids with solids present ✓
- Simple with low capital cost ✓
- Spray formation costs energy ✗
- Liquid can be entrained in gas outlet ✗
- Short liquid residence time ✗



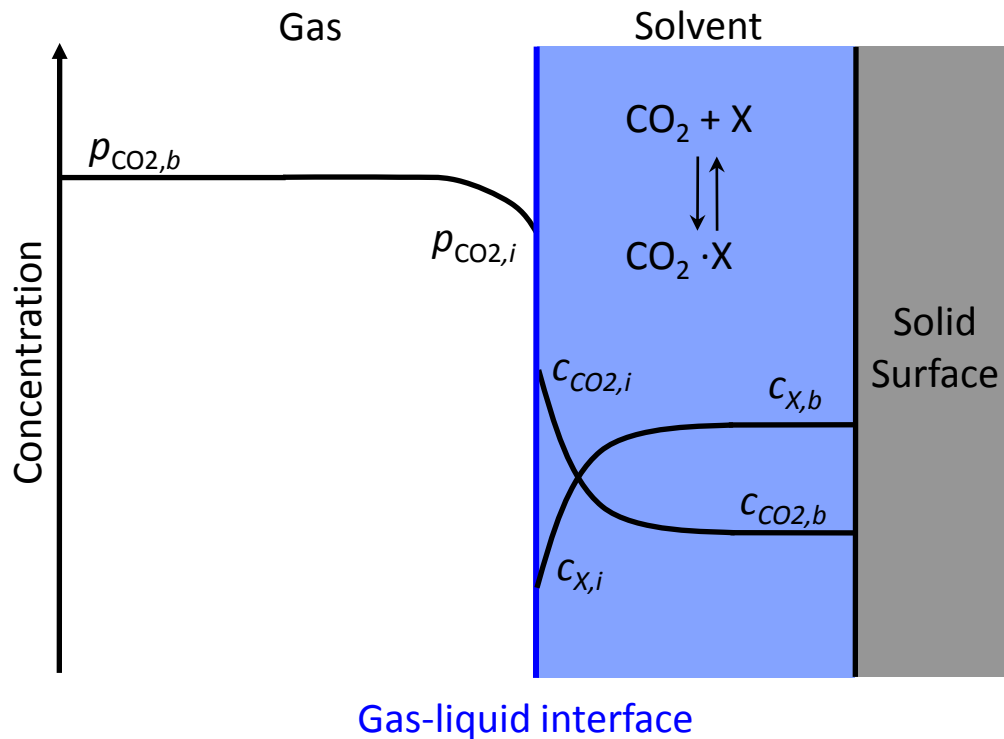
Gas-liquid contacting: BUBBLE COLUMNS

- Large liquid hold-up and long residence time ✓
- Suitable for liquids with solids present ✓
- Simple with low capital cost ✓
- High gas-side pressure drop ✗
- Bubble coalescence ✗



- For post-combustion capture using a chemical absorbent:
 - **Packed columns are favoured due to the low pressure drop and large mass transfer area**
 - Spray columns are also considered due to their simplicity and low cost
- For pre-combustion capture with a physical or chemical absorbent:
 - **Either packed or plate columns can be used due to the sufficient driving force of the high pressure gas stream**
 - Spray columns are not suitable due to liquid entrainment
- Bubble columns are used for gas absorption involving slow reactions and the high pressure drop makes the unattractive for CO₂ capture

Mass transfer in packed columns



Gas-side mass transfer - diffusion

- As the gases in flue gas are unreactive diffusion controls mass transfer on the gas side
- Fick's First and Second Laws:

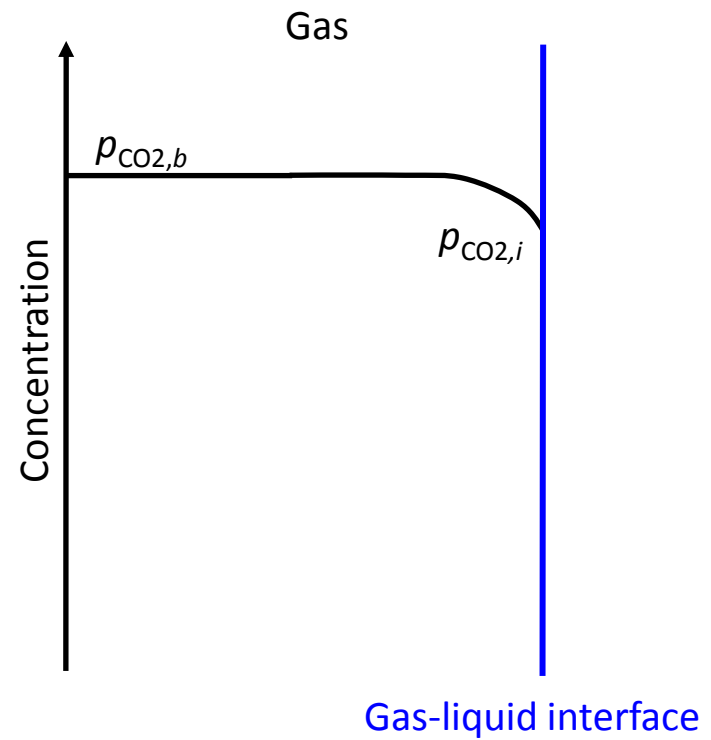
Steady-state
(1st law)

$$N_{CO_2} = D_{CO_2} \frac{\partial c_{CO_2}}{\partial x}$$

$$N_{CO_2} = k_g (p_{CO_2,b} - p_{CO_2,i})$$

$$\frac{\partial c_{CO_2}}{\partial t} = \frac{\partial}{\partial x} \left(D_{CO_2} \frac{\partial c_{CO_2}}{\partial x} \right)$$

Dynamic (2nd
law)



Liquid-side mass transfer – diffusion and reaction

- In the liquid phase both diffusion and reaction controls mass transfer
- Fick's First and Second Laws:

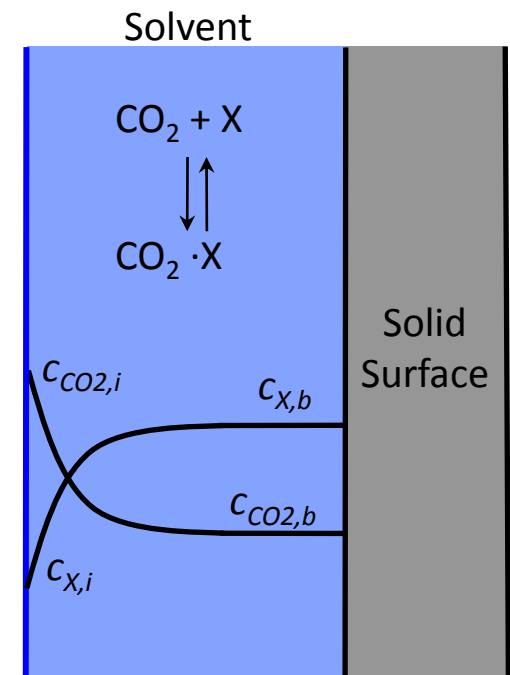
Steady-state
(1st law)

$$N_{\text{CO}_2} = k_l(c_{\text{CO}_2,i} - c_{\text{CO}_2,b})$$

$$\frac{\partial c_{\text{CO}_2}}{\partial t} = D_{\text{CO}_2} \frac{\partial^2 c_{\text{CO}_2}}{\partial x^2} + r$$

$$r = k_f c_{\text{CO}_2} c_X - k_r c_{\text{CO}_2 \cdot X}$$

Dynamic (2nd
law)

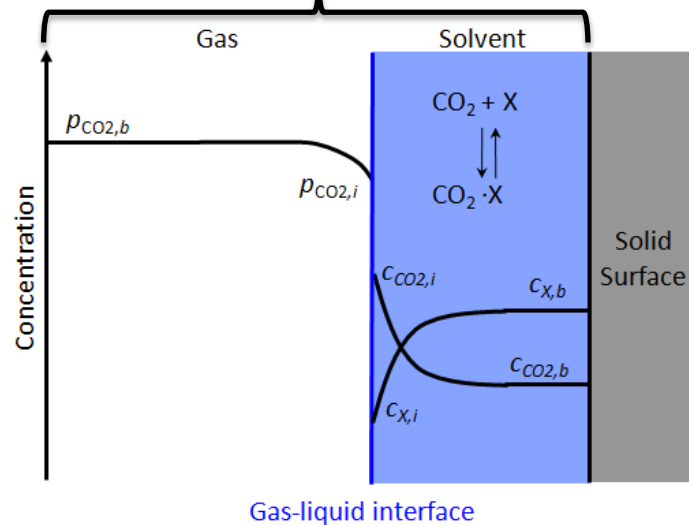


Overall mass transfer

- A combination of gas and liquid side mass transfer, although in packed columns the gas-side can usually be neglected

$$N_{\text{CO}_2} = K_g (p_{\text{CO}_2,b} - k_{h,\text{CO}_2} c_{\text{CO}_2,b})$$

$$\frac{1}{K_g} = \frac{1}{k_g} + \frac{k_{h,\text{CO}_2}}{k_l} \quad k_{h,\text{CO}_2} = \frac{p_{\text{CO}_2}}{c_{\text{CO}_2}}$$



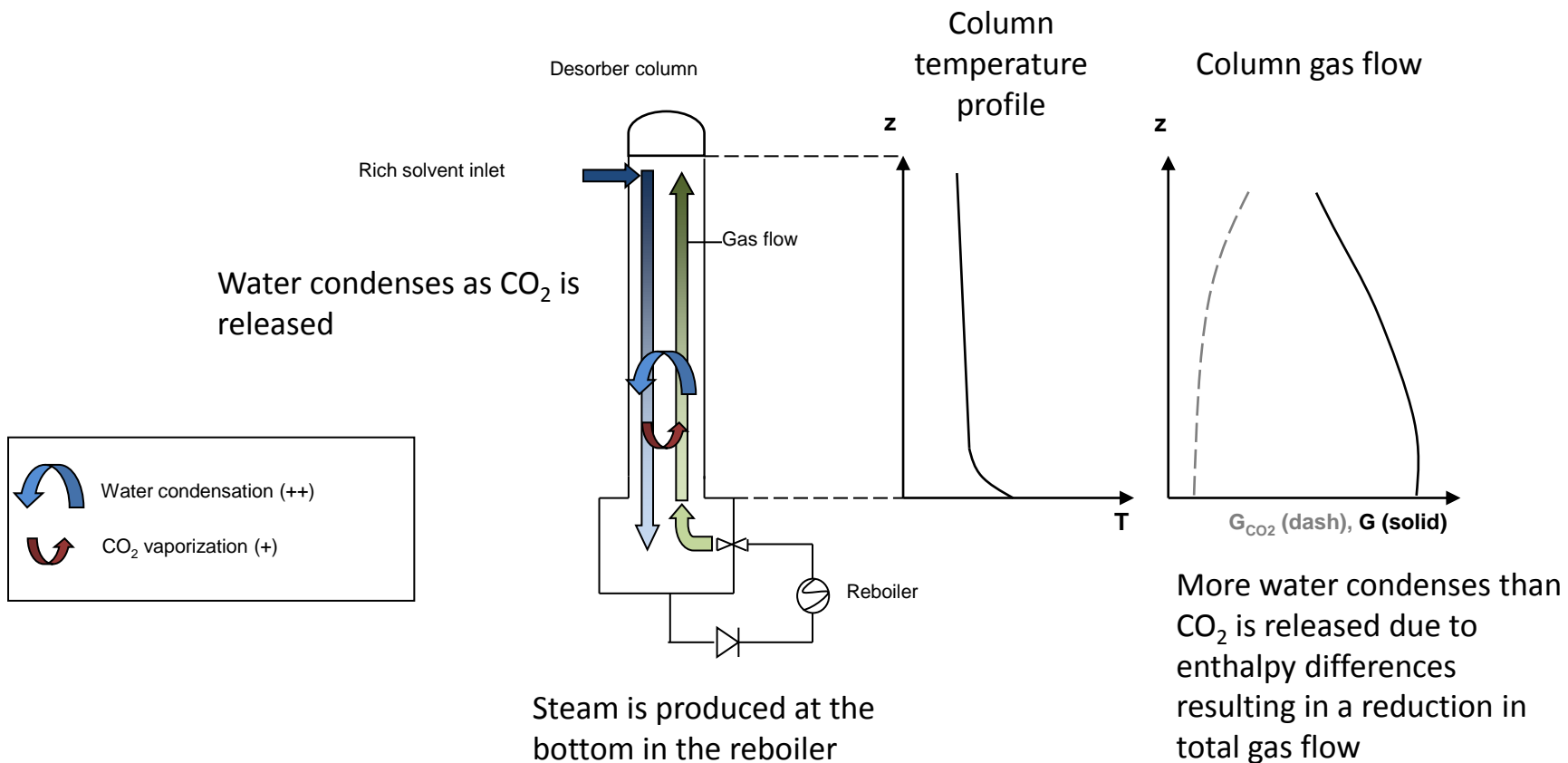
CO₂ stripping

- The CO₂ stripping or desorption process is in many respects the reverse of absorption
- The absorbent is heated to shift the chemical equilibrium position more in favour of CO₂ release
- All of the same mass transfer process apply
- The two main differences in the operation of desorption rather than absorption are:
 - A stripping gas is required to dilute CO₂ and produce a driving force out of solution (and it must be possible to easily separate this stripping gas from CO₂)
 - Desorption is an endothermic process and heat must be applied along the column to maintain the required temperature

CO₂ stripping

- Packed columns are used for CO₂ stripping for the same reasons they are attractive for absorption
- Heat is applied at the base of the stripping column via a reboiler to produce stripping steam
- The stripping steam has two roles:
 - As a stripping gas to dilute CO₂
 - As an energy vector to maintain the column temperature as it condenses along the column
- One of the reasons aqueous solutions are used is that water is a good stripping gas because it can be easily separated from CO₂ by condensation

CO₂ stripping



Acknowledgements

The authors wish to acknowledge financial assistance provided through Australian National Low Emissions Coal Research and Development (ANLEC R&D). ANLEC R&D is supported by Australian Coal Association Low

Emissions Technology Limited and the Australian Government through the Clean Energy Initiative.